

Thermodynamics A work AS1300

① (a) melting Ice cube

Volume of ICE changes as it melts, but mass does not. Thus its a control mass

(b) Air filled into tyre

Both mass and volume changes.
Neither control mass nor a control volume

(c) LPG filled into LPG Cylinder

Volume remains the same. \Rightarrow Control volume

(d) Sand in Sand clock

Control mass.

(e) Spring in a machine

Control mass.

(f) AC

Control volume. Since air is free to move in or out, mass varies

(g) Domestic Refrigerator

Control mass.

(h) Water heated by immersion heater

Control mass.

(i) Water flowing through tap

Control volume.

(j) cloth drying in still air

Control volume

$$d \left(\frac{A_r \rho_u + \lambda u}{Y} \right)$$
$$P \pi R^2 \omega^2 R^2$$

(K) Water drying in a cup

Not CV
Not control mass.

(L) Growing apple

Neither

(M) Air in Air pillow

Control Mass (Volume can change with temperature)

(N) Tube light

Control Mass.

(O) Gas stove burner

Control volume.

(P) Water jet hitting a \perp plate

Control volume.

(Q) Spherical lump of Burning coal.

Neither

(R) Compression in Piston

Control Mass.

(S) Compression in Centrifugal flow compressors

Control volume.

(T) heating in closed chamber

Control Mass.

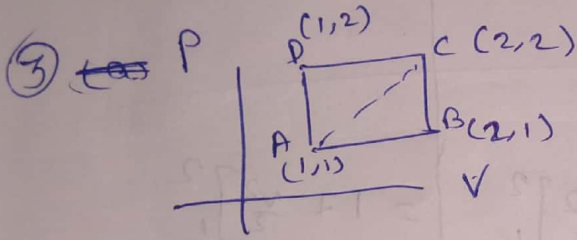
2) Extensive Properties

Depend on the amount of substance.

$$V, E+PV, \frac{PT}{V}, \frac{PV}{T}, \frac{PV}{T^2}$$

Intensive

$$P, T, \frac{PV}{T}$$



$$\int_A^D p dV = 0$$

$$\int_C^D p dV = 0$$

$$\int_A^C p dV = \int_1^2 v dv = \frac{v^2}{2} \Big|_1^2 = \frac{4-1}{2} = 1.5$$

$$\int_B^C p dV = 1$$

$$\int_A^B p dV = 0$$

$$\int_A^D v dp = 1$$

$$\int_C^D v dp = 0$$

$$\int_A^C v dp = 1.5$$

$$\int_B^C v dp = 0$$

$$\int_A^B v dp = 2$$

<u>Path ADc</u>	<u>Path AC</u>	<u>Path ABC</u>
(a) $\int_A^C p dv = \int_A^D p dv + \int_D^C p dv$ $= 0 + 2 = 2$ Path-dependant (Property)	" $= 1.5$	" $= 1$
(b) $\int_{AC} v dp$ $= 1 + 0 = 1$ Path dependant	$= 1.5$	$= 0 + 2 = 2$
(c) $\int (p+v) dv$ $\int_A^C p dv + \int v dv$ $= 2 + \left[\frac{v^2}{2} \right]_1^2 + \left[\frac{v^2}{2} \right]_1^2$ $= 2 + 1.5 = 3.5$ Path dependent	$= 1.5 + \left[\frac{v^2}{2} \right]_1^2$ $= 3$	$= 1 + \left[\frac{v^2}{2} \right]_1^2$ $= 2.5$
(e) $\int p dv + v dp$ $= 2 + 1 = 3$ Path independent	$= 1.5 + 1.5$ $= 3$	$= 1 + 2$ $= 3$
(d) $\int p dv - v dp$ $= 2 - 1 = 1$ Path dependant	$= 0$	$= -1$

$$1.2345678 \times 10^2$$

4 (I)

(a) 90 cm Hg gauge

$$76 \text{ cm Hg} = 1 \text{ atm} = 1.01325 \times 10^5 \text{ Pa}$$

$$90 \text{ cm Hg} \Rightarrow \frac{1.01325 \times 10^5}{76} \times 90 = 119.99 \text{ kPa gauge}$$

Gauge Pressure = Absolute - Atmospheric Pressure

$$\Rightarrow \text{Absolute Pressure} = 221.32 \text{ kPa}$$

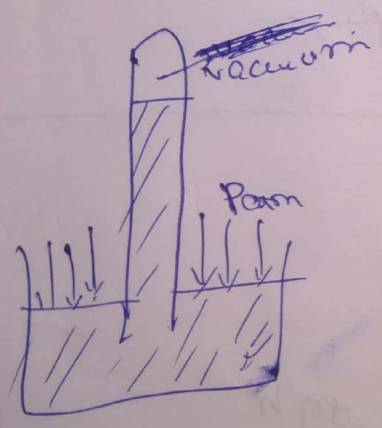
(b) 40 cm Hg vacuum

$$= \frac{1.01325 \times 10^5}{76} \times 40 = 53.33 \text{ kPa vacuum}$$

Vacuum Pressure = Atmospheric Pressure - Absolute Pressure

$$\text{Absolute Pressure} = 101.325 - 53.33 = 47.99 \text{ kPa Absolute}$$

(c) 1m H2O gauge



$$P_{atm} - \rho g h = 0$$

$$h = \frac{1.01325 \times 10^5}{1000 \times 9.81} = 10.33 \text{ m H}_2\text{O}$$

$$1 \text{ atm} = 10.33 \text{ m H}_2\text{O}$$

$$1 \text{ m H}_2\text{O} \Rightarrow \frac{101.325}{10.33} = 9.8 \text{ kPa gauge}$$

$$= 111.13 \text{ kPa absolute}$$

$$= 0.5 \times 101325$$

$$= 50662.5 \text{ Pa}$$

(ii) 0.5 bar absolute

(a) $= -1.01325 + 0.5 = -0.51325 \text{ bar gauge}$

$$= -513.25 \text{ mm Hg gauge}$$

(b) 5 bar absolute

$$= \frac{(5 - 1.01325) \times 10^5}{1.01325 \times 10^5} \times 760$$

$$= 2990.308 \text{ mm Hg gauge}$$

(c) 20 cm Hg absolute

$$(76 - 20) = 56 \text{ cm} = 560 \text{ mm Hg vacuum}$$

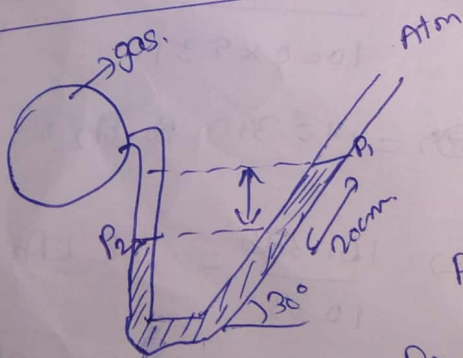
(or)

$$-560 \text{ mm Hg gauge}$$

(d) 800 mm Hg absolute

$$(800 - 760) = 40 \text{ mm Hg gauge}$$

(5)



$$P_1 = P_{atm}$$

$$P_2 = P_{gas}$$

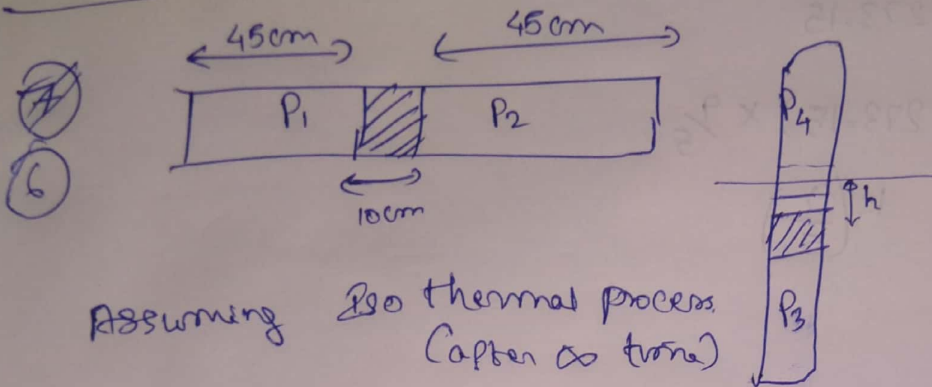
$$P_{gas} - P_{atm} = \rho g h$$

$$P_{gauge} = P_{gas} - P_{atm} = 1000 \times 9.8 \times 0.2 \times \sin 30^\circ$$

$$= 980 \text{ Pa gauge}$$

$$P_{gas} = 101325 + 980 = 102305 \text{ Pa absolute}$$

Absolute Pressure should be used for finding density



Assuming Iso thermal process
(Capten \propto volume)

$$P_1 V_1 = P_2 V_2 = P_3 V_3 = P_4 V_4$$

$$V = A(\text{length})$$

$$45 \times P_1 = (45 - h) P_3 = (45 + h) P_4 \quad \text{--- (1)}$$

$$P_1 = P_{\text{atm}}$$

Force equilibrium

$$P_4 A + A \rho_{\text{mercury}} (10) g = P_3 A$$

$$P_4 + 0.01 \rho g = P_3$$

$$\frac{0.045 P_1}{0.45 + h} + 0.01 \rho g = \frac{0.45 P_1}{(0.45 - h)}$$

$$\Rightarrow 0.045 P_1 \left(\frac{2h}{(0.45)^2 - h^2} \right) = 0.01 \rho g$$

$$\frac{0.045}{0.01} \frac{P_{\text{atm}}}{\rho g} (2h) = (0.45)^2 - h^2$$

$$h^2 + \frac{0.76 \times 0.45 \times 2h}{0.1} - 0.45^2 = 0$$

$$h^2 + 6.84h - 0.2025 = 0$$

$$h = 0.0295 \text{ m}$$

$$h = 2.95 \text{ cm}$$

$$(8) F = c \left(\frac{9}{5} \right) + 32$$

$$c = (F - 32) \frac{5}{9}$$

$$k = c + 273.15$$

$$R = (c + 273.15) \times \frac{9}{5}$$

$$R = k \left(\frac{9}{5} \right)$$

$$(9) c = F$$

$$9c = 5F - 160$$

$$4F = 160$$

$$F = 40$$

$$(b) k = F$$

$$F = (F - 273.15) \frac{9}{5} + 32$$

$$5F = 9F - 2458.35 + 160$$

$$F = 874.5875$$

$$(c) R = c$$

$$5R = (R + 273.15) 9$$

$$-273.15 = 4R$$

$$R = -614.5875 \Rightarrow \text{NOT possible}$$
$$\Rightarrow k < 0$$

$$(d) R = k \text{ at } k = 0$$

(e)

$$R = \left[(R - 32) \frac{5}{9} + 273.15 \right] \frac{9}{5}$$

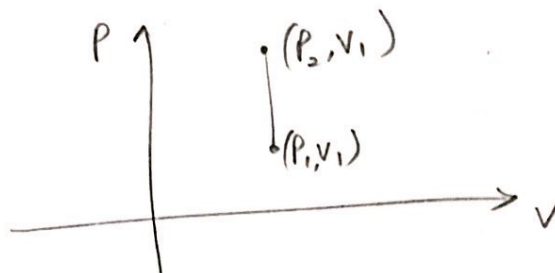
$$R = R - 32 + 273.15 \times \frac{9}{5}$$

NOT possible

7. Derive the work done during the processes.

(a) constant volume (Isochoric process)

$$\Delta V = 0$$



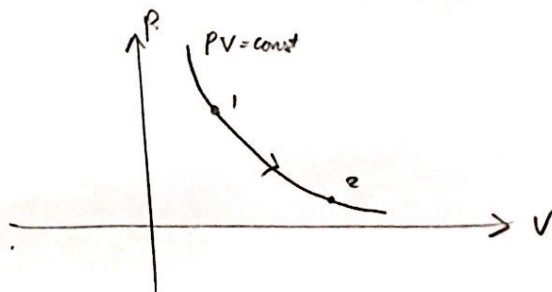
$$\text{Work done: } W = \int_1^2 P dV = 0$$

(b) Isothermal process

$$PV = \text{constant}$$

$$PV = nRT$$

$$W = \int_1^2 P dV = \int_1^2 \frac{nRT}{V} dV = nRT \ln\left(\frac{V_2}{V_1}\right)$$



(c) Polytropic process

$$PV^n = \text{const.} = C$$

$$W = \int_1^2 P dV = C \int_1^2 V^{-n} dV = \frac{P_1 V_1 - P_2 V_2}{n-1}$$

(d) Isobaric process

$$P = \text{constant.}$$

$$W = \int_1^2 P dV = P \Delta V$$

(e) Adiabatic process

$$PV^\gamma = \text{const. (C)}$$

$$W = \frac{P_1 V_1 - P_2 V_2}{\gamma - 1}$$