

# Tutorial 5 Solutions

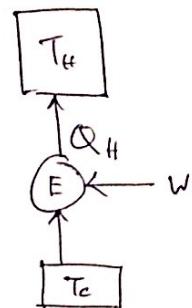
1.

$$T_{amb} = 35^\circ C = 308 K \quad T_{room} = 20^\circ C$$

$$V_{house} = 540 m^3 \times 100$$

$$Q_c = V_{house} \frac{P}{R T} \times C_p \Delta T$$

$$= \frac{540 \times 101325 \times 15 \times 1010}{288.6 \times \underbrace{300}_{\text{average}}} J \\ = 9.57 MJ$$



$$Q_H = Q_c + W$$

$$COP \text{ of ACs} = 3$$

$$W = \frac{Q_c}{3} = 3.19 MJ$$

$$Q_H = 12.77 MJ$$

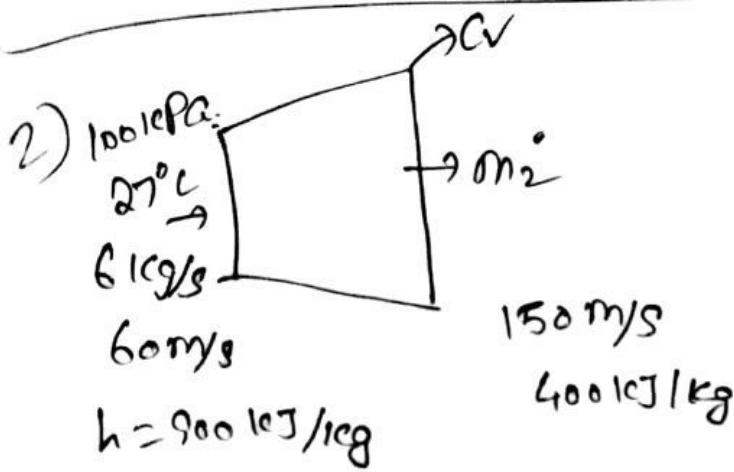
given to  $35^\circ C$  air in volume  $(9290 \times 15 - 70000) m^3$

$$\rho_{out} = \frac{P}{R T} = \frac{101325}{288.6 \times 308} = 1.139 \text{ kg/m}^3$$

$$m_{out} = 1.132 \times 85354 = 97218 \text{ kg}$$

$$\Delta T = \frac{Q_c}{m_{out} C_p} = \frac{12.77 \times 10^6 \times 100}{97218 \times 1010}$$

$$= 13 K$$



$$Q^o = -28 \text{ kJ/kg}$$

Power output = ??

$$Q^o - w^o = \frac{dE_{cv}}{dt} + m_2^o \left( h_2 + \frac{u_2^2}{2} + g_2 \right) - m_1^o \left( h_1 + \frac{u_1^2}{2} + g_2 \right)$$

Neglecting potential energy changes.

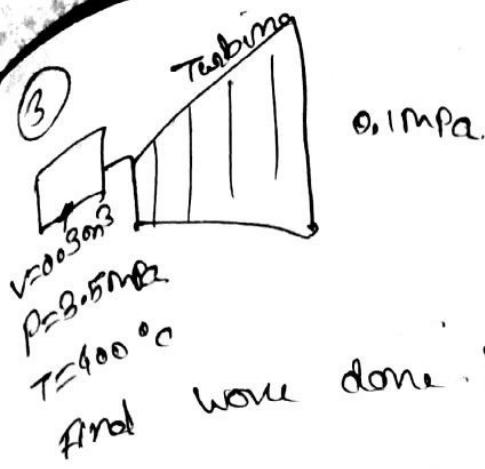
SS state

$$-28 \times \omega^3 \times m^o - w^o = m^o \left( h_2 - h_1 + \frac{u_2^2 - u_1^2}{2} \right)$$

$$w^o = \left[ 28 \times \omega^3 - 400 \times \omega^3 + 900 \times \omega^3 - \frac{150^2}{2} + \frac{60^2}{2} \right] \times 6$$

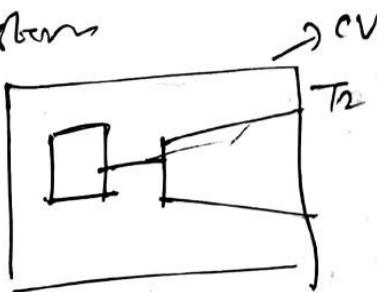
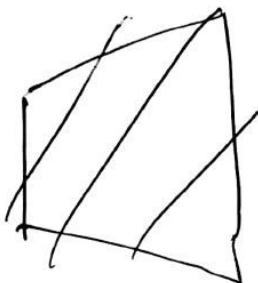
$$w^o = \frac{2775300}{3111300} \text{ Watts}$$

$$\text{Power out} = \frac{3111.3}{2775} \text{ kW}$$



$$W = Q - E$$

lets consider the whole thing as system



$$Q^{\circ} - W^{\circ} = \frac{dE_{cv}}{dt} + m_{out} (h_{out} + \frac{u^2}{2} + \gamma z)$$

Neglecting heat transfer

$$-W^{\circ} = \frac{dE_{cv}}{dt} + m_{out} (cp) T_2$$

Neglecting the volume occupied by Turbine.

$T_2 \Rightarrow$  atmospheric temperature (constant)

Integrate

~~$$W = E_2 - E_1$$~~

$$-W = E_f - E_i + m_{out} (cp) T_2$$

$$-W = m_f(v) T_f - m_i(c_v T_i) + (m_f - m_i) cp T_2$$

$T_i = 400^\circ \text{ C}$   
Adiabatic expansion  $\Rightarrow$

$$\frac{(400 + 273)}{(3.5 \times 10^6)^{1/1.4}} = \frac{T_2}{(0.1 \times 10^6)^{1/1.4}}$$

$$\Rightarrow T_2 = 248.698 \text{ K}$$

Airflow stops when pressure difference becomes zero.

$$(P_f)_{cv} = P_2 = 0.1 \text{ atm MPa}$$

$\Rightarrow$  final temperature.

$$\left( \frac{(T_f)_{cv}}{(0.1)^{\gamma-1}} \right)^{\frac{1}{\gamma}} = \left( \frac{T_2}{(0.1)} \right)^{\frac{1}{\gamma-1}}$$

$$\Rightarrow (T_f)_{cv} = T_2 = 243.7$$

$$m_f = (\rho) V$$

$$= \frac{\rho}{RT} V$$

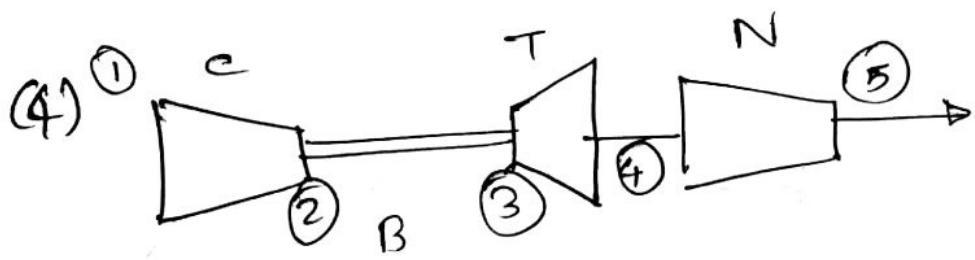
$$m_f = \frac{0.1 \times 10^6}{288 \times 243.7} \times 0.3 = 0.427 \text{ kg}$$

$$m_i = \frac{3.5 \times 10^6}{288 \times 673} \times 0.3 = 5.417 \text{ kg}$$

$$-W = (0.427 \times 717.85 \times 243.7 - 5.417 \times 717.85) \times 673$$

$$\cancel{\Phi} (0.427 - 5.417)(1005)(243.7)$$

$$W = 1317.384 \text{ kJ}$$



$$\dot{m}^{\circ} = w_0 \text{ kg/s}$$

$$T_1 = T_a = 300 \text{ K}$$

$$P_1 = 1 \text{ atm}$$

$$P_2 = 18 \text{ atm}$$

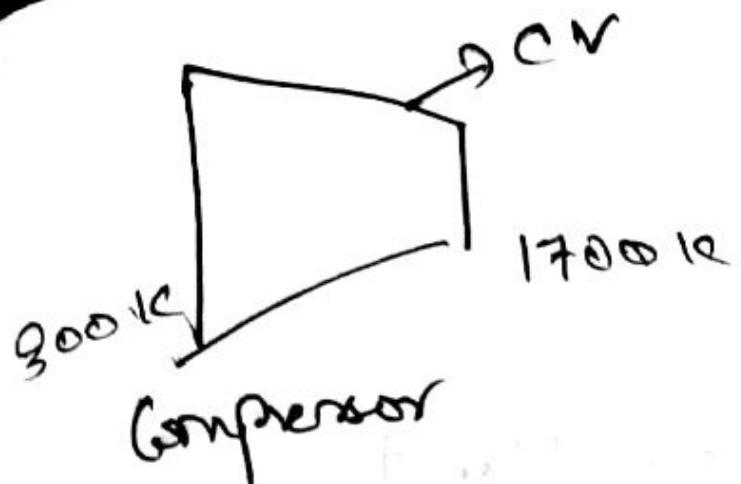
$$T_3 = 1700 \text{ K}$$

$$Q^{\circ} - W^{\circ} = \frac{dEcv}{dt} + m_{\text{out}} (h_{\text{out}} + \frac{u^2}{2} + g z_{\text{out}}) - m_{\text{in}} (h_{\text{in}} + \frac{u_{\text{in}}^2}{2} + g z_{\text{in}})$$

~~T<sub>5</sub> ??~~

T<sub>4</sub> ??

To get T<sub>4</sub> we need the enthalpy of gas at 4. Which requires Work done extracted by Turbine that depends on Compressor



Neglecting the inlet velocity

Igeniusropic Compressor  $\Rightarrow Q^0 = 0$

~~-~~ $\cancel{Q^0}$  Steady state  $\Rightarrow \frac{dE}{dt} = 0$

$T_2$  is not known!

Assuming  
membrane compression  
 $p_{\text{N}_2}$  = constant

$$P = fRT$$

$$P \left( \frac{RT}{P} \right)^{\gamma} = \text{constant}$$

$$\frac{T_1^{\gamma}}{P_1^{\gamma-1}} = \frac{T_2^{\gamma}}{P_2^{\gamma-1}}$$

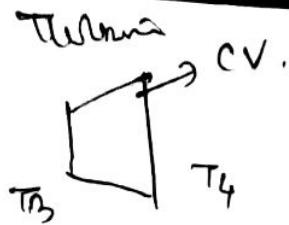
$$(300) \times \left( \frac{18}{1} \right)^{\gamma-1} = T_2^{\gamma}$$

$\gamma = 1.4$

$$T_2 = 685 \text{ K}$$

$$-w^o = m^o(h_2 - h_1) \quad \cancel{= 100}$$

$$w^o = -100 \times 1005 \times (685 - 300) = -38,673 \text{ mw}$$



$$T_3 = 1700 \text{ K}$$

Work done by Compressor on Fluid.

= Work done by Fluid on Turbine

$$-W^o_{\text{fluid}} = m^o C_p (T_4 - T_3)$$

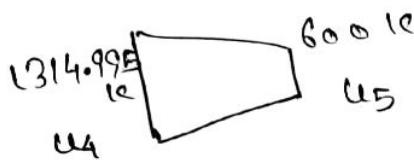
on turbine 100

$$\textcircled{N} = 100 \times 1005 (T_4 - 1700) = -38.693 \times 10^6$$

$$T_4 = 1700 - \frac{38.693 \times 10^6}{100 \times 1005}$$

$$T_4 = 1314.995 \text{ K}$$

### Nozzle



Assume  $u_4 \ll u_5$

$$Q^o = 0$$

$$W^o = 0$$

Steady state.

$$h_4 + \frac{u_4^2}{2} = h_5 + \frac{u_5^2}{2}$$

$$C_p (T_4 - T_5) = \frac{u_5^2}{2}$$

$$u_5 = \sqrt{2(1005)(1314.995 - 600)}$$

$$u_5 = 1198 \text{ m/s}$$

5)

$$w_1 = w_2$$

$$Q_h - Q = Q - Q_c$$

$$\frac{Q_h}{Q} - 1 = 1 - \frac{Q_c}{Q}$$

$$\frac{T_h}{T} - 1 = 1 - \frac{T_c}{T} \Rightarrow$$

$$\boxed{T = \frac{T_h + T_c}{2}}$$

1 b) when  $\gamma_1 = \gamma_2$

$$1 - \frac{Q}{Q_h} = 1 - \frac{Q_c}{Q}$$

$$1 - \frac{\tau}{\tau_h} = 1 - \frac{\tau_c}{\tau_0}$$

$$\Rightarrow \tau = \sqrt{\tau_c \tau_0}$$